

## Case – 18 Gas Analysis

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### Case Background:

The compressors in any of refrigeration systems are actually performing gas compression function no matter what type of refrigerant is used for the refrigeration system. The refrigerant can be halocarbons, ammonia or hydrocarbons. In most cases, the refrigerant used for refrigeration system only consists of one gas component. For example, R-290 is 100% of propane, R-1270 is 100% of propylene, etc.

Sometime, for pipe line gas compression or in some case the refrigerant used for process refrigeration system is a mixed hydrocarbon, which consists of many gas components instead of pure refrigerant.

This case is to demonstrate the method to calculate the properties of the gas mixture.

# Related Technical Data and Engineering Information for the Case:

No.	Compound	Formula	Molecular weight	Boiling point, °F., 14.696 psia	Vapor pressure, 100°F., psia	Freezing point, °F., 14.696 psia	Critical constants		
							Pressure, psia	Temperature, °F.	Volume, cu ft/lb
1	Methane	CH <sub>4</sub>	16.043	-258.69	(5000)	-296.46 <sup>d</sup>	667.8	-116.63	0.0991
2	Ethane	C <sub>2</sub> H <sub>6</sub>	30.070	-127.48	(800)	-297.89 <sup>d</sup>	707.8	90.09	0.0788
3	Propane	C <sub>3</sub> H <sub>8</sub>	44.097	-43.67	190.	-305.84 <sup>d</sup>	616.3	206.01	0.0737
4	n-Butane	C <sub>4</sub> H <sub>10</sub>	58.124	31.10	51.6	-217.05	550.7	305.65	0.0702
5	Isobutane	C <sub>4</sub> H <sub>10</sub>	58.124	10.90	72.2	-255.29	529.1	274.98	0.0724
6	n-Pentane	C <sub>5</sub> H <sub>12</sub>	72.151	96.92	15.570	-201.51	488.6	385.7	0.0675
7	Isopentane	C <sub>5</sub> H <sub>12</sub>	72.151	82.12	20.44	-255.83	490.4	369.10	0.0679
8	Neopentane	C <sub>5</sub> H <sub>12</sub>	72.151	49.10	35.9	2.17	464.0	321.13	0.0674
9	n-Hexane	C <sub>6</sub> H <sub>14</sub>	86.178	155.72	4.956	-139.58	436.9	453.7	0.0688
10	2-Methylpentane	C <sub>6</sub> H <sub>14</sub>	86.178	140.47	6.767	-244.63	436.6	435.83	0.0681
11	3-Methylpentane	C <sub>6</sub> H <sub>14</sub>	86.178	145.89	6.098	—	453.1	448.3	0.0681
12	Neohexane	C <sub>6</sub> H <sub>14</sub>	86.178	121.52	9.856	-147.72	446.8	420.13	0.0667
13	2,3-Dimethylbutane	C <sub>6</sub> H <sub>14</sub>	86.178	136.36	7.404	-199.38	453.5	440.29	0.0665
14	n-Heptane	C <sub>7</sub> H <sub>16</sub>	100.205	209.17	1.620	-131.05	396.8	512.8	0.0691
15	2-Methylhexane	C <sub>7</sub> H <sub>16</sub>	100.205	194.09	2.271	-180.89	396.5	495.00	0.0673
16	3-Methylhexane	C <sub>7</sub> H <sub>16</sub>	100.205	197.32	2.130	—	408.1	503.78	0.0646
17	3-Ethylhexane	C <sub>7</sub> H <sub>16</sub>	100.205	200.25	2.012	-181.48	419.3	513.48	0.0665
18	2,2-Dimethylpentane	C <sub>7</sub> H <sub>16</sub>	100.205	174.54	3.492	-190.86	402.2	477.23	0.0665
19	2,4-Dimethylpentane	C <sub>7</sub> H <sub>16</sub>	100.205	176.89	3.292	-182.63	396.9	475.95	0.0668
20	3,3-Dimethylpentane	C <sub>7</sub> H <sub>16</sub>	100.205	186.91	2.773	-210.01	427.2	505.85	0.0662
21	Triptane	C <sub>7</sub> H <sub>16</sub>	100.205	177.58	3.374	-12.82	428.4	496.44	0.0636
22	n-Octane	C <sub>8</sub> H <sub>18</sub>	114.232	258.22	0.537	-70.18	360.6	564.22	0.0690
23	Diisobutyl	C <sub>8</sub> H <sub>18</sub>	114.232	228.39	1.101	-132.07	360.6	530.44	0.0676
24	Isooctane	C <sub>8</sub> H <sub>18</sub>	114.232	210.63	1.708	-161.27	372.4	519.46	0.0656
25	n-Nonane	C <sub>9</sub> H <sub>20</sub>	128.259	303.47	0.179	-64.28	332.	610.68	0.0684
26	n-Decane	C <sub>10</sub> H <sub>22</sub>	142.286	345.48	0.0597	-21.36	304.	652.1	0.0679
27	Cyclopentane	C <sub>5</sub> H <sub>10</sub>	70.125	120.65	9.914	-136.91	653.9	461.5	0.059
28	Methylcyclopentane	C <sub>6</sub> H <sub>12</sub>	84.162	161.25	4.503	-224.44	548.9	499.35	0.0607
29	Cyclohexane	C <sub>6</sub> H <sub>12</sub>	84.162	177.29	3.264	43.77	591.	536.7	0.0586
30	Methylcyclohexane	C <sub>7</sub> H <sub>14</sub>	98.189	213.68	1.609	-195.87	503.5	570.27	0.0600
31	Ethylene	C <sub>2</sub> H <sub>4</sub>	28.054	-154.62	—	-272.45 <sup>d</sup>	729.8	48.58	0.0737
32	Propene	C <sub>3</sub> H <sub>6</sub>	42.081	-53.90	226.4	-301.45 <sup>d</sup>	669.	196.9	0.0689
33	1-Butene	C <sub>4</sub> H <sub>8</sub>	56.108	20.75	63.05	-301.63 <sup>d</sup>	583.	295.6	0.0685
34	Cis-2-Butene	C <sub>4</sub> H <sub>8</sub>	56.108	38.69	45.54	-218.06	610.	324.37	0.0668
35	Trans-2-Butene	C <sub>4</sub> H <sub>8</sub>	56.108	33.58	49.80	-157.96	595.	311.86	0.0680
36	Isobutene	C <sub>4</sub> H <sub>8</sub>	56.108	19.59	63.40	-220.61	580.	292.55	0.0682
37	1-Pentene	C <sub>5</sub> H <sub>10</sub>	70.135	85.93	19.115	-265.39	590.	376.93	0.0697
38	1,2-Butadiene	C <sub>4</sub> H <sub>6</sub>	54.092	51.53	(20.)	-213.16	(653.)	(339.)	(0.0649)
39	1,3-Butadiene	C <sub>4</sub> H <sub>6</sub>	54.092	24.06	(60.)	-164.02	628.	306.	0.0654
40	Isoprene	C <sub>5</sub> H <sub>8</sub>	68.119	93.30	16.672	-230.74	(558.4)	(412.)	(0.0650)
41	Acetylene	C <sub>2</sub> H <sub>2</sub>	26.038	-119*	—	-114.*	890.4	95.31	0.0695
42	Benzene	C <sub>6</sub> H <sub>6</sub>	78.114	176.17	3.224	41.96	710.4	552.22	0.0531
43	Toluene	C <sub>7</sub> H <sub>8</sub>	92.141	231.13	1.032	-138.94	595.9	605.55	0.0549
44	Ethylbenzene	C <sub>8</sub> H <sub>10</sub>	106.168	277.16	0.371	-138.91	523.5	651.24	0.0564
45	o-Xylene	C <sub>8</sub> H <sub>10</sub>	106.168	291.97	0.264	-13.30	541.4	675.0	0.0557
46	m-Xylene	C <sub>8</sub> H <sub>10</sub>	106.168	282.41	0.326	-54.12	513.6	651.02	0.0567
47	p-Xylene	C <sub>8</sub> H <sub>10</sub>	106.168	281.05	0.342	55.66	509.2	649.6	0.0572
48	Styrene	C <sub>8</sub> H <sub>8</sub>	104.152	293.29	(0.24)	-23.10	580.	706.0	0.0541
49	Isopropylbenzene	C <sub>9</sub> H <sub>12</sub>	120.195	306.34	0.188	-140.82	465.4	676.4	0.0570
50	Methyl Alcohol	CH <sub>3</sub> O	32.042	148.1(2)	4.63(22)	-143.82(22)	1174.2(21)	462.97(21)	0.0589(21)
51	Ethyl Alcohol	C <sub>2</sub> H <sub>5</sub> O	46.069	172.92(22)	2.3(7)	-173.4(22)	925.3(21)	469.58(21)	0.0580(21)
52	Carbon Monoxide	CO	28.010	-313.6(2)	—	-340.6(2)	507.(17)	-220.(17)	0.0532(17)
53	Carbon Dioxide	CO <sub>2</sub>	44.010	-109.3(2)	—	—	1071.(17)	-87.9(23)	0.0342(23)
54	Hydrogen Sulfide	H <sub>2</sub> S	34.076	-76.6(24)	394.0(6)	-117.2(7)	1306.(17)	212.7(17)	0.0459(24)
55	Sulfur Dioxide	SO <sub>2</sub>	64.059	14.0(7)	88.(7)	-103.9(7)	1145.(24)	315.5(17)	0.0306(24)
56	Ammonia	NH <sub>3</sub>	17.031	-28.2(24)	212.(7)	-107.9(2)	1636.(17)	270.3(24)	0.0681(17)
57	Air	N <sub>2</sub> O <sub>2</sub>	28.964	-317.6(2)	—	—	547.(2)	-221.3(2)	0.0517(3)
58	Hydrogen	H <sub>2</sub>	2.016	-423.0(24)	—	-434.8(24)	188.1(17)	-399.8(17)	0.0516(24)
59	Oxygen	O <sub>2</sub>	31.999	-297.4(2)	—	-361.8(24)	736.9(24)	-181.1(17)	0.0382(24)
60	Nitrogen	N <sub>2</sub>	28.013	-320.4(2)	—	-346.0(24)	493.0(24)	-232.4(24)	0.0514(17)
61	Chlorine	Cl <sub>2</sub>	70.906	-29.3(24)	158.(7)	-149.8(24)	1118.4(24)	291.(17)	0.0281(17)
62	Water	H <sub>2</sub> O	18.015	212.0	0.9492(12)	32.0	3208.(17)	705.6(17)	0.0500(17)
63	Helium	He	4.003	—	—	—	—	—	—
64	Hydrogen Chloride	HCl	36.461	-121.16	925.(7)	-173.6(16)	1198.(17)	124.5(17)	0.0208(17)

Figure 18-1 Physical Constants of Various Hydrocarbons

°F	H <sub>2</sub>	N <sub>2</sub>	O <sub>2</sub>	CO	CO <sub>2</sub>	H <sub>2</sub> O	H <sub>2</sub> S	SO <sub>2</sub>	SO <sub>3</sub>	CH <sub>4</sub>	C <sub>2</sub> H <sub>2</sub>	°F
-300	6.93	6.94	6.95	6.95	7.00					7.95		-300
-290	6.83	6.94	6.95	6.95	7.01					7.95		-290
-280	6.73	6.94	6.95	6.95	7.02					7.95		-280
-270	6.64	6.94	6.95	6.95	7.04					7.95		-270
-260	6.57	6.95	6.95	6.95	7.06					7.95		-260
-250	6.51	6.95	6.95	6.95	7.08					7.95		-250
-240	6.46	6.95	6.95	6.95	7.10					7.95		-240
-230	6.42	6.95	6.95	6.95	7.12					7.95		-230
-220	6.38	6.95	6.95	6.95	7.15					7.95		-220
-210	6.36	6.95	6.95	6.95	7.17					7.95		-210
-200	6.35	6.95	6.95	6.95	7.20		7.88	8.10	9.00	7.95		-200
-190	6.34	6.95	6.95	6.95	7.25		7.88	8.14	9.11	7.95		-190
-180	6.35	6.95	6.95	6.95	7.28		7.90	8.20	9.22	7.95		-180
-170	6.36	6.95	6.95	6.95	7.32		7.90	8.24	9.33	7.95		-170
-160	6.39	6.95	6.95	6.95	7.37		7.91	8.30	9.45	7.96		-160
-150	6.42	6.95	6.95	6.95	7.42		7.92	8.35	9.56	7.96		-150
-140	6.44	6.95	6.95	6.95	7.47		7.93	8.40	9.67	7.96		-140
-130	6.47	6.95	6.95	6.95	7.53		7.94	8.45	9.77	7.97		-130
-120	6.50	6.95	6.96	6.95	7.59		7.95	8.50	9.90	7.98		-120
-110	6.53	6.95	6.96	6.95	7.65		7.96	8.56	10.0	7.99		-110
-100	6.56	6.95	6.96	6.95	7.71		7.97	8.61	10.1	8.00		-100
-90	6.58	6.95	6.96	6.95	7.78		7.98	8.66	10.2	8.02		-90
-80	6.61	6.95	6.96	6.95	7.84		7.99	8.71	10.3	8.04		-80
-70	6.63	6.95	6.96	6.95	7.90		8.00	8.76	10.4	8.06		-70
-60	6.66	6.95	6.96	6.95	7.97		8.02	8.81	10.6	8.08		-60
-50	6.68	6.95	6.96	6.95	8.03		8.03	8.87	10.7	8.09		-50
-40	6.70	6.95	6.97	6.95	8.11		8.04	8.91	10.8	8.12		-40
-30	6.72	6.95	6.97	6.95	8.18		8.05	8.97	10.9	8.15		-30
-20	6.75	6.95	6.97	6.95	8.25		8.06	9.01	11.0	8.17		-20
-10	6.77	6.95	6.97	6.95	8.33		8.07	9.06	11.1	8.20		-10
0	6.78	6.95	6.98	6.95	8.38	7.88	8.09	9.12	11.2	8.23	9.68	0
10	6.80	6.95	6.98	6.95	8.45	7.99	8.10	9.18	11.3	8.26	9.79	10
20	6.82	6.95	6.98	6.95	8.51	7.99	8.12	9.23	11.4	8.29	9.90	20
30	6.83	6.95	6.99	6.96	8.58	8.00	8.13	9.28	11.6	8.33	10.0	30
40	6.85	6.95	6.99	6.96	8.65	8.00	8.15	9.33	11.7	8.37	10.1	40
50	6.86	6.95	7.00	6.96	8.70	8.00	8.16	9.38	11.8	8.41	10.2	50
60	6.87	6.95	7.00	6.96	8.76	8.01	8.17	9.43	11.9	8.45	10.3	60
70	6.88	6.95	7.01	6.95	8.83	8.02	8.19	9.48	12.0	8.49	10.4	70
80	6.89	6.96	7.02	6.96	8.89	8.02	8.20	9.53	12.1	8.54	10.5	80
90	6.90	6.96	7.02	6.96	8.95	8.03	8.22	9.59	12.2	8.59	10.6	90
100	6.90	6.96	7.03	6.96	9.01	8.03	8.24	9.64	12.3	8.65	10.7	100
110	6.91	6.96	7.03	6.96	9.06	8.04	8.25	9.69	12.4	8.70	10.8	110
120	6.92	6.96	7.04	6.97	9.12	8.05	8.27	9.74	12.6	8.76	10.9	120
130	6.92	6.96	7.05	6.97	9.19	8.06	8.28	9.79	12.7	8.82	11.0	130
140	6.93	6.96	7.06	6.97	9.24	8.06	8.30	9.84	12.8	8.86	11.1	140
150	6.93	6.96	7.07	6.97	9.30	8.07	8.32	9.88	12.9	8.95	11.1	150
160	6.94	6.96	7.08	6.97	9.35	8.08	8.34	9.94	13.0	9.01	11.2	160
170	6.94	6.96	7.09	6.98	9.40	8.09	8.36	9.98	13.1	9.08	11.3	170
180	6.94	6.96	7.10	6.98	9.46	8.10	8.38	10.0	13.2	9.14	11.4	180
190	6.95	6.96	7.11	6.98	9.51	8.11	8.39	10.1	13.3	9.21	11.5	190

Figure 18-2 Values of Various Ideal Gases Mol. Wt. Cp – Btu/Lb-Mole-° F

*F	C <sub>2</sub> H <sub>4</sub>	C <sub>2</sub> H <sub>6</sub>	C <sub>3</sub> H <sub>6</sub>	C <sub>3</sub> H <sub>8</sub>	iC <sub>4</sub> H <sub>8</sub>	1C <sub>4</sub> H <sub>8</sub>	iC <sub>4</sub> H <sub>10</sub>	nC <sub>4</sub> H <sub>10</sub>	iC <sub>5</sub> H <sub>12</sub>	nC <sub>5</sub> H <sub>12</sub>	nC <sub>6</sub> H <sub>14</sub>	nC <sub>7</sub> H <sub>16</sub>	*F
-300	8.13	8.51	9.17	9.45			10.5	12.6					-300
-290	8.13	8.55	9.28	9.61			10.8	12.8					-290
-280	8.13	8.60	9.37	9.80			11.1	13.0					-280
-270	8.13	8.66	9.48	9.98			11.5	13.3					-270
-260	8.13	8.71	9.60	10.2			11.8	13.5					-260
-250	8.13	8.77	9.72	10.4			12.1	13.8					-250
-240	8.13	8.84	9.85	10.5			12.5	14.1					-240
-230	8.14	8.90	10.0	10.7			12.8	14.4					-230
-220	8.14	8.98	10.1	10.9			13.1	14.7					-220
-210	8.15	9.06	10.3	11.1			13.5	15.0					-210
-200	8.15	9.14	10.4	11.3			13.8	15.2					-200
-190	8.16	9.23	10.6	11.5			14.2	15.5					-190
-180	8.17	9.32	10.7	11.7			14.5	15.8					-180
-170	8.19	9.41	10.9	11.9			14.8	16.1					-170
-160	8.20	9.51	11.0	12.1			15.2	16.4					-160
-150	8.22	9.61	11.2	12.3			15.5	16.7					-150
-140	8.24	9.72	11.4	12.5			15.8	17.0					-140
-130	8.26	9.82	11.5	12.7			16.2	17.3					-130
-120	8.29	9.94	11.7	12.9			16.5	17.7					-120
-110	8.33	10.0	11.9	13.1			16.8	18.0					-110
-100	8.37	10.2	12.0	13.3	15.8	15.2	17.2	18.3	19.9	20.6	25.1	29.2	-100
-90	8.42	10.3	12.2	13.6	16.1	15.4	17.5	18.6	20.4	21.1	25.6	29.8	-90
-80	8.48	10.4	12.4	13.8	16.4	15.6	17.8	18.9	20.9	21.5	26.1	30.4	-80
-70	8.55	10.5	12.5	14.0	16.7	15.9	18.1	19.2	21.4	22.0	26.6	30.9	-70
-60	8.64	10.6	12.7	14.2	17.1	16.1	18.4	19.5	21.9	22.5	27.1	31.5	-60
-50	8.72	10.8	12.9	14.5	17.4	16.4	18.7	19.8	22.3	22.9	27.7	32.1	-50
-40	8.82	10.9	13.1	14.7	17.7	16.7	19.0	20.1	22.8	23.4	28.2	32.7	-40
-30	8.92	11.1	13.2	14.9	18.0	17.0	19.4	20.4	23.3	23.8	28.7	33.3	-30
-20	9.04	11.2	13.4	15.2	18.3	17.3	19.7	20.7	23.8	24.3	29.2	33.9	-20
-10	9.17	11.3	13.6	15.4	18.6	17.6	20.1	21.0	24.3	24.8	29.7	34.5	-10
0	9.32	11.4	13.7	15.6	18.9	18.0	20.4	21.3	24.8	25.2	30.2	35.1	0
10	9.46	11.6	13.8	15.9	19.2	18.3	20.7	21.5	25.2	25.7	30.7	35.7	10
20	9.60	11.7	14.1	16.1	19.5	18.6	21.1	21.8	25.7	26.2	31.3	36.3	20
30	9.74	11.9	14.3	16.4	19.9	19.0	21.5	22.1	26.2	26.6	31.8	36.9	30
40	9.88	12.0	14.5	16.6	20.2	19.3	21.8	22.4	26.6	27.0	32.3	37.5	40
50	10.0	12.2	14.7	16.9	20.5	19.6	22.2	22.6	27.1	27.5	32.8	38.1	50
60	10.2	12.3	14.9	17.1	20.8	19.9	22.5	22.9	27.6	27.9	33.3	38.7	60
70	10.3	12.5	15.1	17.4	21.1	20.2	22.9	23.2	28.0	28.4	33.8	39.3	70
80	10.4	12.6	15.3	17.6	21.4	20.5	23.2	23.4	28.5	28.8	34.4	39.8	80
90	10.6	12.8	15.5	17.9	21.6	20.9	23.6	23.7	28.9	29.3	34.9	40.4	90
100	10.7	13.0	15.8	18.2	22.0	21.2	24.0	24.1	29.4	29.7	35.4	41.1	100
110	10.9	13.1	16.0	18.4	22.2	21.5	24.3	24.4	29.8	30.1	35.9	41.7	110
120	11.0	13.3	16.2	18.7	22.5	21.8	24.7	24.8	30.3	30.6	36.4	42.2	120
130	11.1	13.4	16.4	19.0	22.8	22.1	25.0	25.1	30.8	31.0	37.0	42.8	130
140	11.3	13.6	16.6	19.2	23.1	22.4	25.4	25.5	31.2	31.5	37.5	43.4	140
150	11.4	13.8	16.8	19.5	23.4	22.7	25.8	25.8	31.7	31.9	38.0	44.0	150
160	11.5	13.9	17.0	19.8	23.7	23.0	26.1	26.1	32.1	32.3	38.5	44.6	160
170	11.7	14.1	17.2	20.1	24.0	23.3	26.5	26.5	32.6	32.7	39.0	45.2	170
180	11.8	14.3	17.4	20.4	24.3	23.6	26.9	26.9	33.0	33.2	39.5	45.8	180
190	11.9	14.5	17.6	20.6	24.6	24.0	27.2	27.2	33.4	33.6	40.0	46.4	190

Figure 18-3 Values of Various Ideal Gases Mol. Wt. Cp – Btu/Lb-Mole-°F

## Cogitation

When making gas compression calculation, the gas physical properties such as molecular weight, critical pressure, critical temperature and the Mol. Wt. Cp. of a gas mixture required are required. If the gas is a mixture of various hydrocarbons, a calculation shall be made to find out the properties of the gas mixture. Each components of the gas mixture must be given either by percent of moles or percent of weight. If the percentages are given by percents weight, it shall be converted to percents.

The Figure 18-1 is the physical properties table for molecular weight, critical pressure, critical temperature for most of the hydrocarbon gases. The Figure 18-2 and 18-2 are the Mol. Wt. Cp at various temperatures for the hydrocarbon gases.

Figure 18-1 also shows the formula each of the hydrocarbons. Sometimes, hydrocarbon gas is expressed with numerical prefix, such as C<sub>1</sub> for Methane, C<sub>2</sub> for Ethane, iC<sub>4</sub> fir Iso-Butane and etc, numerical prefix for gases are shown as the following:

C <sub>n</sub>		iC <sub>n</sub> - Iso		nC <sub>n</sub> - Normal			
Examples:							
n		n		n			
1	Methane	12	Dodecane	22	Docosane	32	Dotriacontane
2	Ethane	13	Tridecane	23	Tricosane	33	Tritriacontane
3	Propane	14	Tetradecane	24	Tetracosane	40	Tetracontane
4	Butane	15	Pentadecane	25	Pentacosane	50	Pentacontane
5	Pentane	16	Hexadecane	26	Hexacosane	60	Hexacontane
6	Hexane	17	Heptadecane	27	Heptacosane	70	Heptacontane
7	Heptane	18	Octadecane	28	Octacosane	80	Octacontane
8	Octane	19	Nonadecane	29	Nonacosane	90	Nonacontane
9	Nonane	20	Eicosane	30	Triacontane	100	Hectane
10	Decane	21	Heneicosane	31	Hentriacontane	132	Dotriacontahecta
11	Undecane						

The following is the demonstration to show how to calculate the physical properties of a gas mixture:

Gas properties calculation for gas mixture when mole% is given:

### 1.0 Mixture of gases:

For a mixture of gas, the exact value of Mole Percent or Weight Percent must be provided for each components of the gas composition; undefined expressions such as 'Others', 'Approximately', Misc. Gases' and etc are not allowed. Therefore, the following undefined gas composition expression is not to be used:

Methane	89%
Ethane	4%
Propane	5%
Others	2%

The following gas composition expression is acceptable:

Methane	89%
Ethane	4%
Propane	5%
Carbon.Dioxide	2%

## 2.0 Chemical Formula, Mole Percents and M.F. for the mixture:

		Mole%	M.F.
Methane	CH <sub>4</sub>	89%	0.89
Ethane	C <sub>2</sub> H <sub>6</sub>	4%	0.04
Propane	C <sub>3</sub> H <sub>8</sub>	5%	0.05
Carb..Dioxide	CO <sub>2</sub>	2%	0.02
Total		100%	1.00

The total must be exactly equal to 100% mole percent or 1.00 for M.F.

## 3.0 Physical constants of the each components from Figure 18-1:

Methane, CH <sub>4</sub>	Molecular Weight = 16.043 Critical Pressure = 667.8 Psia Critical Temp = -116.63°F Or °R = -116.63 + 460 = 343.37°R MWcp at 80°F = 8.54
Ethane, C <sub>2</sub> H <sub>6</sub>	Molecular Weight = 30.07 Critical Pressure = 707.8 Psia Critical Temp = 90.09°F Or °R = 90.09 + 460 = 550.1°R MWcp at 80°F = 12.6
Propane, C <sub>3</sub> H <sub>8</sub>	Molecular Weight = 44.-97 Critical Pressure = 616.3 Psia Critical Temp = 206.01°F Or °R = 206.01 + 460 = 666.0°R MWcp at 80°F = 17.6
Carbon Dioxide	Molecular Weight = 44.01 Critical Pressure = 1071 Psia Critical Temp = 87.9°F Or °R = 87.9 + 460 = 547.9°R MWcp at 80°F = 8.89

#### 4.0 To calculate the Molecular Weight for the Gas Mixture:

The pseudo M.W. of Methane =  $16.0 \times 0.89 = 14.24$ .

Follow the same steps to calculate the partial M.W. for other component of the gas.

Component	Formula	M.W.	Mol %	Pseudo M.W.
Methane	CH <sub>4</sub>	16.0	89%	14.24
Ethane	C <sub>2</sub> H <sub>6</sub>	30.1	4%	1.20
Propane	C <sub>3</sub> H <sub>8</sub>	44.1	5%	2.21
Carb.Dioxide	CO <sub>2</sub>	44.0	2%	0.88
Mixture Gas			100%	18.53

Therefore, the Molecular Weight of the gas mixture is 18.53

#### 5.0 To calculate the Critical Pressure (Psia) for the gas mixture:

The Pseudo Critical Pressure of Methane =  $667.8 \times 0.89 = 594.34$ .

Follow the same steps to calculate the partial critical pressure for other component of the gas.

Component	Formula	Mol %	Critical Press.	Pseudo Critical Press.
Methane	CH <sub>4</sub>	89%	667.8	594.34
Ethane	C <sub>2</sub> H <sub>6</sub>	4%	707.8	28.31
Propane	C <sub>3</sub> H <sub>8</sub>	5%	616.3	30.82
Carb.Dioxide	CO <sub>2</sub>	2%	1071	21.42
Mixture Gas		100%		674.89

Therefore, the critical pressure of the gas mixture is 674.79 Psia

#### 6.0 To Calculate the Critical Temperature for the Gas Mixture:

Temperature used for gas compression calculation is Rankin Temperature °R instead of °F; so change all the °F to °R to calculate the mixture critical temperature.

The Pseudo Critical Temperature of Methane =  $343.37 \times 0.89 = 305.60$ .

Follow the same steps to calculate the partial critical temperature for other component of the gas.

Component	Formula	Mol %	Critical Temperature	Pseudo Temp. °R
Methane	CH <sub>4</sub>	89%	$(-116.63 + 460) = 343.37$	305.60
Ethane	C <sub>2</sub> H <sub>6</sub>	4%	$(90.09 + 460) = 550.09$	22.00
Propane	C <sub>3</sub> H <sub>8</sub>	5%	$(206.01 + 460) = 666.01$	33.30
Carb.Dioxide	CO <sub>2</sub>	2%	$(87.9 + 460) = 547.90$	10.96
Mixture Gas		100%		371.86

Therefore, the Critical Temperature of the Gas Mixture is 371.86°R

## 7.0 To Calculate the Mol. Wt. Cp for the Gas Mixture:

The MW<sub>c</sub>p is to be used for the calculation of the k factor. It is always associated with the temperature at the suction. Assuming the operating condition is 80°F, the example is to calculate the MW<sub>c</sub>p of the gas mixture at 80°F at compressor suction.

The Pseudo MW<sub>c</sub>p of Methane =  $8.54 \times 0.89 = 7.60$ .

Follow the same steps to calculate the partial MW<sub>c</sub>p for other component of the gas.

Component	Formula	Mol %.	MW <sub>c</sub> p	MW <sub>c</sub> p
Methane	CH <sub>4</sub>	89%	8.54	7.600
Ethane	C <sub>2</sub> H <sub>6</sub>	4%	12.60	0.504
Propane	C <sub>3</sub> H <sub>8</sub>	5%	17.6	0.880
Carb.Dioxide	CO <sub>2</sub>	2%	8.89	0.178
Mixture Gas		100%		9.162

Therefore, the MW<sub>c</sub>p of the Gas Mixture at 80°F is 9.162

## 8.0 Gas Analysis Table:

Component	Formula	M.W.	Mol %	Pseudo M.W.	Critical Press.	Critical Temp.	MW <sub>c</sub> p	Component Pseudo		
								Press.	Temp.	MW <sub>c</sub> p
Methane	CH <sub>4</sub>	16.0	89%	14.24	668	343	8.54	595	305	7.600
Ethane	C <sub>2</sub> H <sub>6</sub>	30.1	4%	1.20	708	550	12.60	28	22	0.504
Propane	C <sub>3</sub> H <sub>8</sub>	44.1	5%	2.21	616	666	17.6	31	33	0.880
Carb.Dioxide	CO <sub>2</sub>	44.0	2%	0.88	1071	548	8.89	21	11	0.178
Mixture Gas			100%	18.53				675	371	9.162



Therefore, physical properties of the gas mixture are as the following:

MW of gas mixture:	18.53
Critical Pressure:	675 Psia
Critical Temperature:	371°R
MWcp at 80°F:	9.162

### Converting Weight Percents to Mole Percent for gas mixture:

As indicated earlier, the properties calculation for gas mixture are based on Mole%, therefore, if only Wt% is given for the gas flow, the Wt% should be converted into Mol% in order to calculate the gas properties of the mixture. The steps to convert the Wt% to Mol% are as the following:

#### (1) Components of mixture gas, Wt% given:

Propane	C <sub>3</sub> H <sub>8</sub>	75.90% by weight
Methane	CH <sub>4</sub>	8.48%
Ethane	C <sub>2</sub> H <sub>6</sub>	7.95%
n-Butan	n-C <sub>4</sub> H <sub>10</sub>	7.67%

#### (2) Find the molecular weight of each component of the gas:

		Molecular weight
Propane	C <sub>3</sub> H <sub>8</sub>	44.094
Methane	CH <sub>4</sub>	16.042
Ethane	C <sub>2</sub> H <sub>6</sub>	30.068
n-Butan	n-C <sub>4</sub> H <sub>10</sub>	58.120

#### (3) Convert the Weight Percent to Mole Percent:

Calculate the Mol Gas per 100# of Mixture for Propane component:

$$= \frac{\text{Wt}\%}{\text{MW}} = \frac{75.90}{44.094} = 1.7213$$

Same step to calculate the value for other gas components and the result is as the following:

	MW	Wt%	Mol Gas Per 100# Mix.
Propane, C <sub>3</sub> H <sub>8</sub>	44.094	75.90	1.7213
Methane, CH <sub>4</sub>	16.042	8.48	0.5286
Ethane , C <sub>2</sub> H <sub>6</sub>	30.068	7.95	0.2644
n-Butan, n-C <sub>4</sub> H <sub>10</sub>	58.120	7.67	0.1320
		100.00%	2.6463

Total Lb. Mol per 100 Lbs gas is 2.6463

$$\text{Mol\% for Propane gas} = \frac{1.7213}{2.6463} = 65.05 \text{ Mol\%}$$

Follow the same steps to calculate the Mole% for other gas component and the result is shown below:

	MW	Wt%	Mol Gas Per 100# Mix.	Mol %
Propane, C <sub>3</sub> H <sub>8</sub>	44.094	75.90	1.7213	65.05
Methane, CH <sub>4</sub>	16.042	8.48	0.5286	19.98
Ethane , C <sub>2</sub> H <sub>6</sub>	30.068	7.95	0.2644	9.99
n-Butan, n-C <sub>4</sub> H <sub>10</sub>	58.120	7.67	0.1320	4.98
		100.00%	2.6463	100.0%

**(4) Gas mixture in Mole percent:**

Propane	C <sub>3</sub> H <sub>8</sub>	65.05% by Mole
Methane	CH <sub>4</sub>	19.98%
Ethane	C <sub>2</sub> H <sub>6</sub>	9.99%
n-Butan	n-C <sub>4</sub> H <sub>10</sub>	4.98%